

powder that was converted into gas, which amounted 14.4 kg/hr.

TABLE IV
COLD GAS EFFICIENCY ANALYSIS OF AUTO-THERMAL CONVERSION PROCESS

Parameter	Inlet		Outlet
	Tar	Coal powder	Combustible gas
Flow (kg/hr)	20	14.4	84.52
Calorific Value (Cal/g)	8,560.72	5,293	783.62
Energy (kCal/hr)	175,545.45	76,219.25	66,228.21
	251,764.75		
Cold Gas Efficiency (%)	26.31		

IV. CONCLUSION

An experiment on combustible gas generation from co-gasification of tar and coal powder was conducted in an auto-thermal reactor to determine the temperature of the process, combustible gas composition, and efficiency of the process. From calculation and experiments about oxidizing reactor operation, 20 kg/hr tar was more promising to operate and can reach the optimal temperature which was 1,900°C. The energy from oxidizing reactor used for the reduction reaction of tar and pyrolysis of coal powder and produce combustible yield gas. Coal powder was fed into the reformer reactor and will be pyrolyzed into fuel gas and charcoal. The coal powder that can be conversion was about 14.4 kg/hr and produce approximately 84.52 kg/hr combustible gas. The calorific value of combustible yield gas amounted to 783.62 Cal/g. It still can be improved by increasing the gas content of carbon monoxide (CO) and reduce carbon dioxide (CO₂) through the reduction reaction of CO₂ to CO in the reactor reductants. Combustible yield gas has advantages levels of hydrogen gas (H₂) as high as 19.2%, which is already exceeding the levels of hydrogen gas from coal gasification is only <10%. Hydrogen gas is the fuel that is environmentally friendly because it does not produce the greenhouse effect. This is due to feed tar has a chemical composition ratio H/C which is higher than coal. Cold gas efficiency (CGE) has a value which was still low at 26.31% compared to gasification which have efficiency 50-70. It is caused by two factors, namely the calorific value fuel gas produced was still low and the remainder of the conversion of coal powder were still mostly in the form of charcoal.

ACKNOWLEDGMENT

The authors would like to thank the R&D Center for Mineral and Coal Technology (tekMIRA), Ministry of Energy and Mineral Resources, who has funded this research.

REFERENCES

- [1] M. Faizal, "Utilization Biomass and Coal Mixture to Produce Alternative Solid Fuel for Reducing Emission of Green House Gas," *International Journal on Advanced Science, Engineering and Information Technology*, vol. 7, no. 3, pp. 950–956, 2017.
- [2] P. Gilbert, C. Ryu, V. Sharifi, and J. Swithenbank, "Tar reduction in pyrolysis vapors from biomass over a hot char bed," *Bioresour. Technol.*, vol. 100, no. 23, pp. 6045–6051, 2009.
- [3] M. P. Houben, H. C. De Lange, and a. a. Van Steenhoven, "Tar reduction through partial combustion of fuel gas," *Fuel*, vol. 84, no. 7–8, pp. 817–824, 2005.
- [4] D. Singh, E. Hernández-Pacheco, P. N. Hutton, N. Patel, and M. D. Mann, "Carbon deposition in an SOFC fueled by tar-laden biomass gas: A thermodynamic analysis," *J. Power Sources*, vol. 142, no. 1–2, pp. 194–199, 2005.
- [5] J. Han and H. Kim, "The reduction and control technology of tar during biomass gasification/pyrolysis: An overview," *Renew. Sustain. Energy Rev.*, vol. 12, no. 2, pp. 397–416, 2008.
- [6] G. Stravinskias and V. Grigaitien, "Comparison of steam reforming and partial oxidation of biomass pyrolysis tars over activated carbon derived from the waste tire," vol. 196, pp. 67–74, 2012.
- [7] M. Ma, M. Mu, J. Richter, R. Kriegel, D. Bo, and N. Ruhe, "Investigation of combined catalyst and oxygen carrier systems for the partial oxidation of naphthalene as model tar from biomass gasification," vol. 3, pp. 1–7, 2012.
- [8] J. Ahrenfeldt, H. Egsgaard, W. Stelte, T. Thomsen, and U. B. Henriksen, "The influence of partial oxidation mechanisms on tar destruction in TwoStage biomass gasification," *Fuel*, vol. 112, pp. 662–680, 2013.
- [9] M. Ma and M. Müller, "Applied Catalysis A : General Investigation of various catalysts for partial oxidation of tar from biomass gasification," *Applied Catal. A, Gen.*, vol. 493, pp. 121–128, 2015.
- [10] Y. Tsuboi, S. Ito, M. Takafuji, H. Ohara, and T. Fujimori, "Development of a regenerative reformer for tar-free syngas production in a steam gasification process," *Appl. Energy*, no. x, 2016.
- [11] S. Zhao, Y. Luo, Y. Zhang, and Y. Long, "Journal of Analytical and Applied Pyrolysis Experimental investigation of the synergy effect of partial oxidation and bio-char on biomass tar reduction," *J. Anal. Appl. Pyrolysis*, vol. 112, pp. 262–269, 2015.
- [12] T. A. Van Der Hoeven, H. C. De Lange, and A. A. Van Steenhoven, "Analysis of hydrogen-influence on tar removal by partial oxidation," vol. 85, pp. 1101–1110, 2006.
- [13] M. Higman, C. and van der Burgt, "Gasification: The Thermodynamics of Gasification," 2nd ed., Elsevier, 2008.
- [14] L. Cundari, L. Nurul Komariah, N. Novia, I. Maretha, and L. Septiana, "Temperature Distribution of Biodiesel Blends Combustion in Boiler using CFD-Fluent," *International Journal on Advanced Science, Engineering and Information Technology*, vol. 6, no. 1, pp. 120–123, 2016.
- [15] L. F. De Diego, M. De Obras-Ioscertales, A. Rufas, P. Gayán, A. Abad, and J. Adánez, "Pollutant emissions in a bubbling fluidized bed combustor working in oxy-fuel operating conditions : Effect of flue gas recirculation," *Appl. Energy*, vol. 102, no. x, pp. 860–867, 2013.
- [16] M. De Obras-Ioscertales, T. Mendiara, A. Rufas, L. F. De Diego, P. Gayán, A. Abad, and J. Adánez, "NO and N2O emissions in oxy-fuel combustion of coal in a bubbling fluidized bed combustor," *Fuel*, vol. 150, pp. 146–153, 2015.
- [17] C. M. Kalamaras and A. M. Efstathiou, "Hydrogen Production Technologies : Current State and Future Developments," vol. 2013, 2013.
- [18] M. A. Andriansyah Efendi, and N. Nurhadi, "Comparison of an Internal Combustion Engine Derating Operated on Producer Gas from Coal and Biomass Gasification," *International Journal on Advanced Science, Engineering and Information Technology*, vol. 6, no. 3, pp. 385–389, 2016.